

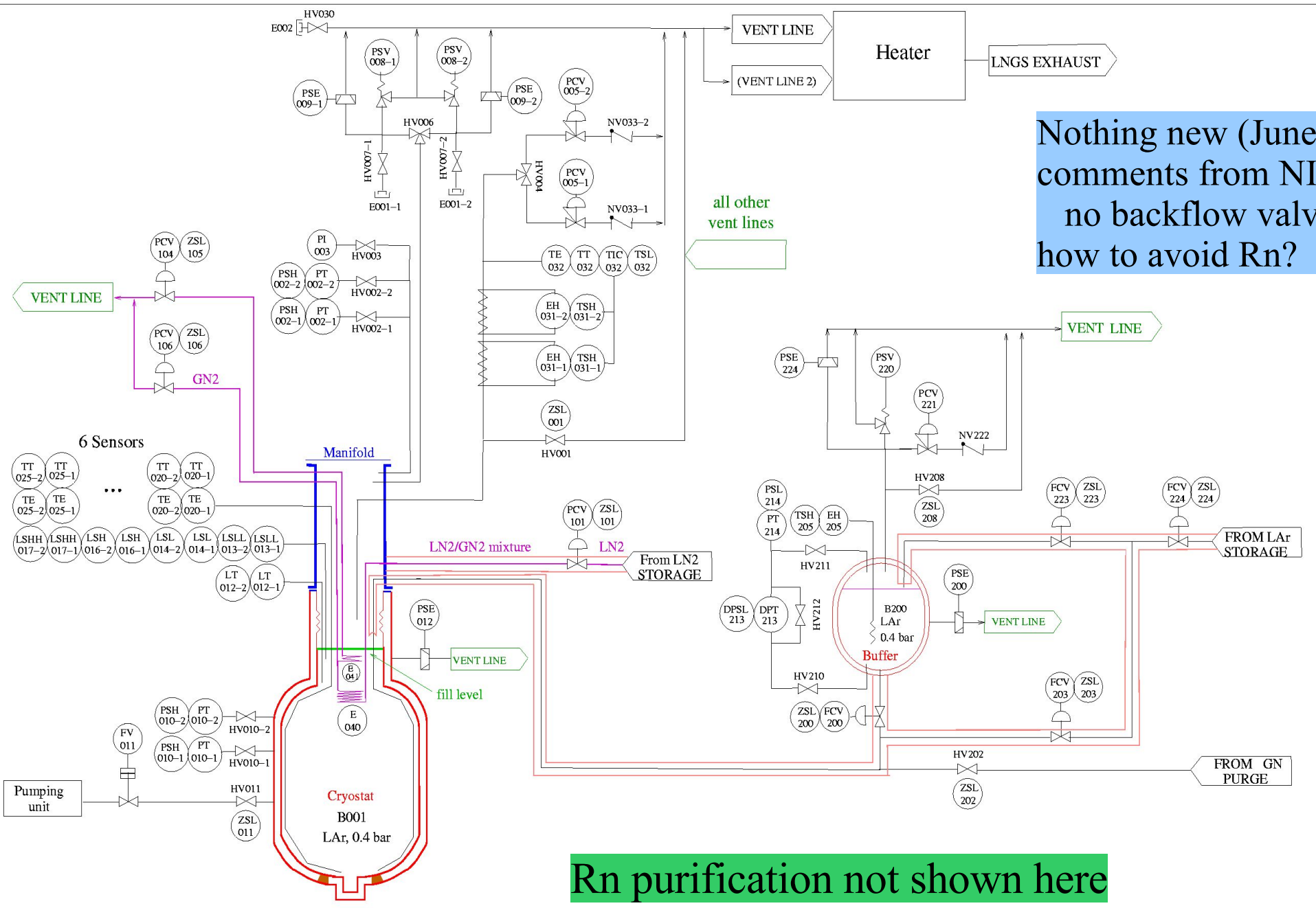
Cryogenic Infrastructure

Bernhard Schwingenheuer, MPIK Heidelberg

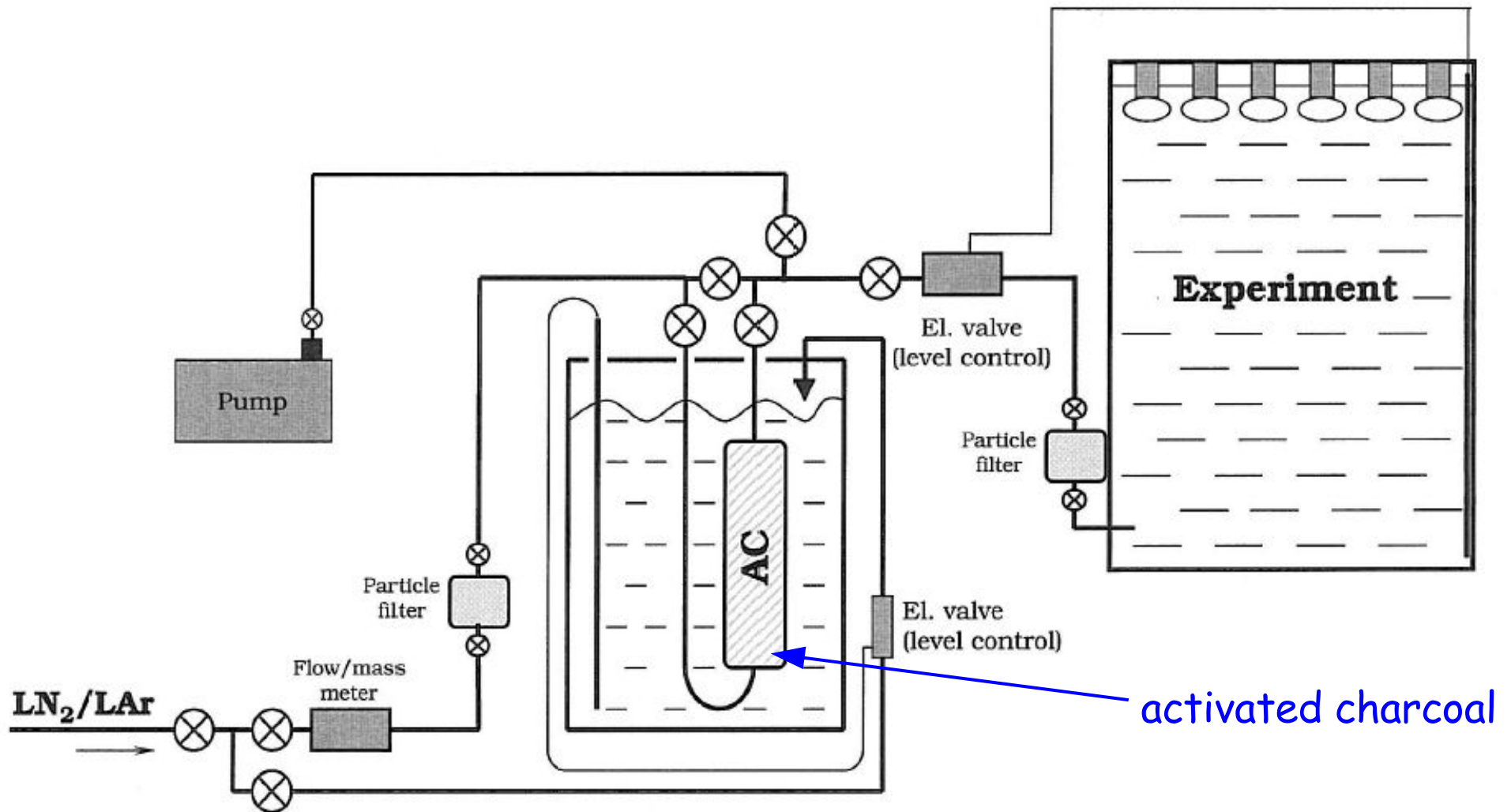
Content

- reminder of PID drawing for cryostat
- cryogenic control valves
- exhaust gas heating
- interface to Penthouse gas system
- tender

Piping and Instrumentation Design



Radon purification plant



consensus: want a small unit for refilling,
design needs optimization (valves,...) & integration into PID

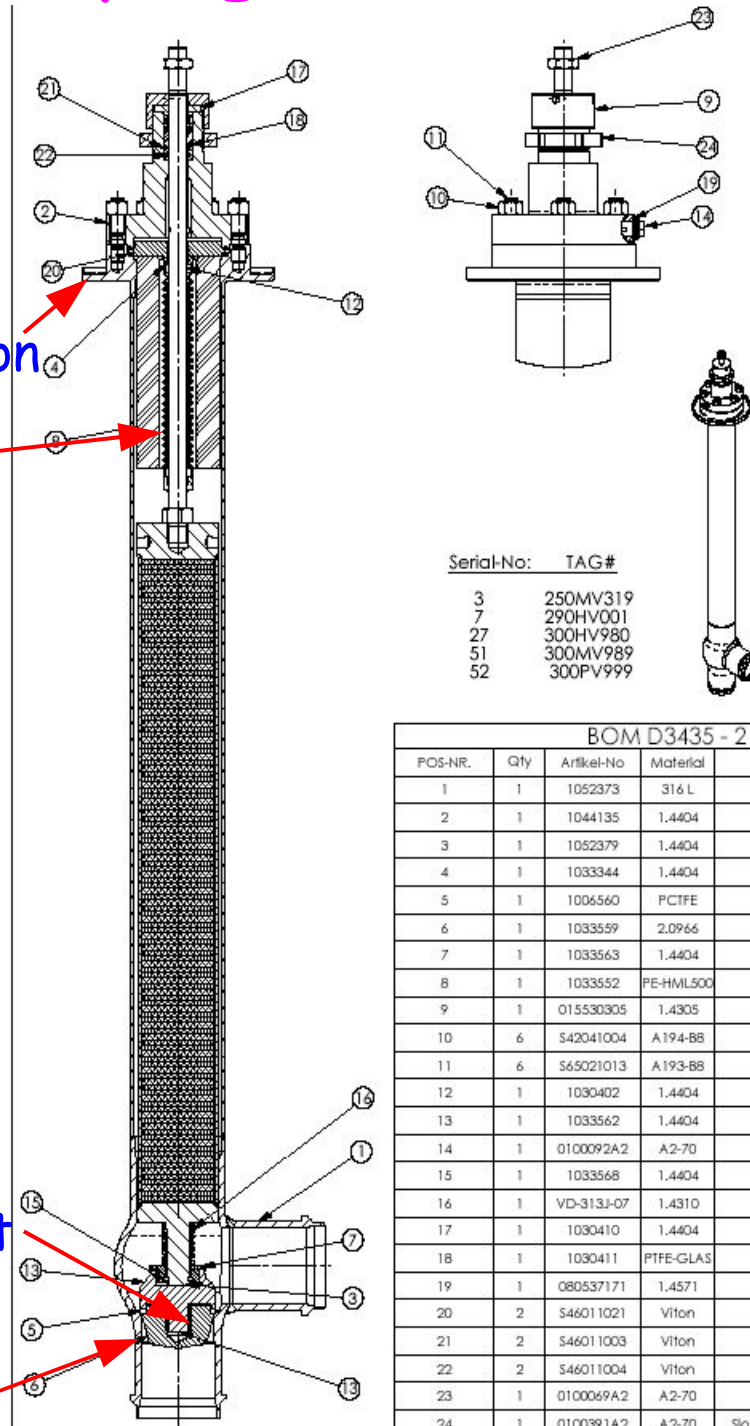
Cryogenic Control Valves

cold box connection

bellow

soft seat gasket

Al-brass plug



BOM		30 bar	Cryogenic Valve		Scale 1:3
Dr-Ho	Material	PN Class	DN Size	DN 3	Project
2 1/2"	2 1/2"	30 bar	2 1/2"	1052388	1052388
Weight (kg)	3059.513	Dr-Ho	Material	PN Class	DN Size
Dr-Ho	Material	PN Class	DN Size	DN 3	Project
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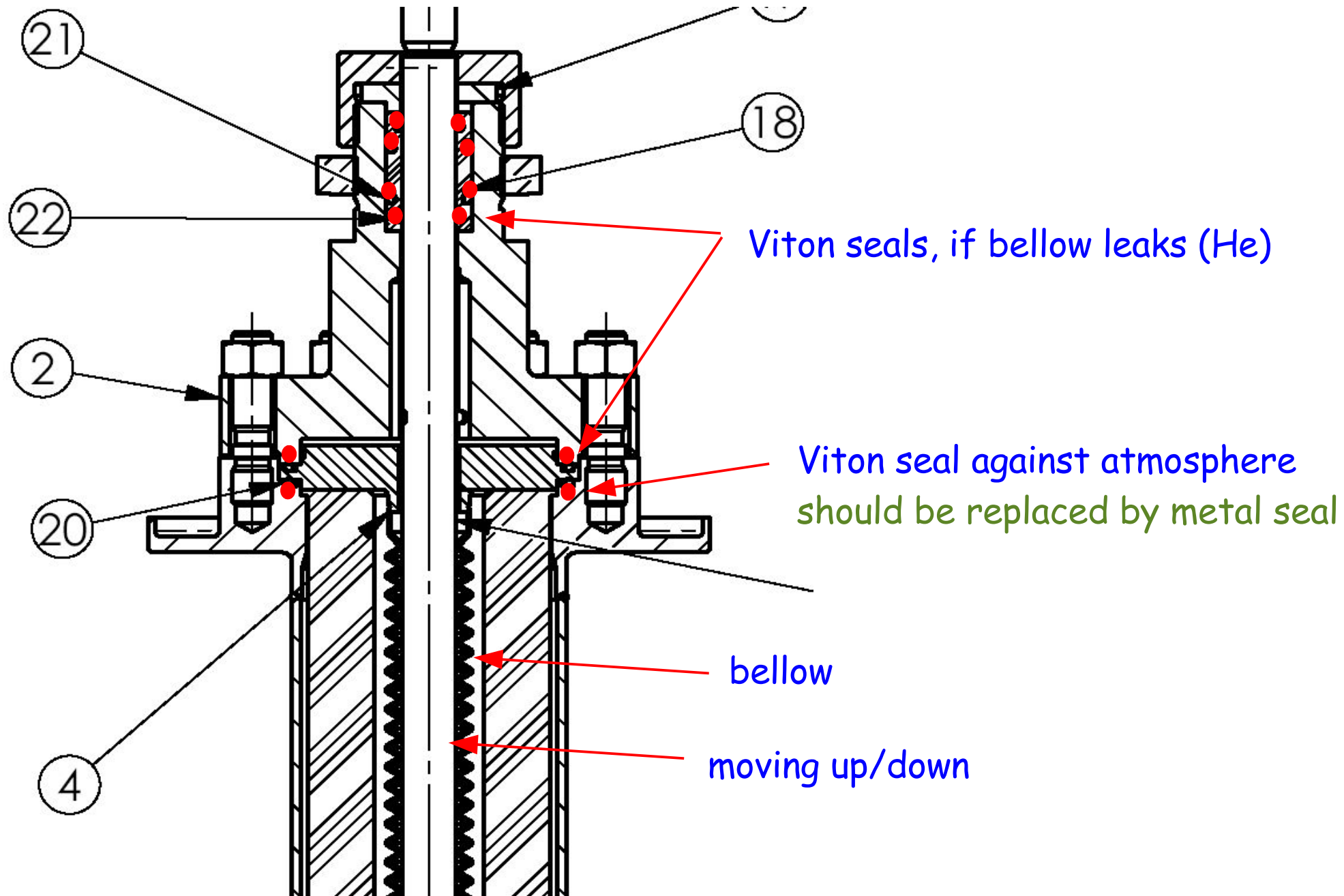
what do we want?

- radon tight against atmosphere, how?
- open/close or linear flow regulator
- cross section ?
- vacuum insulated ?
- metall or soft (PCTFE, Vespel) seat?
- screwed or welded?

what is available?

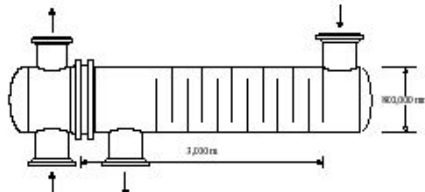
- lots of valuable help by G. Perinic, CERN
- discussion with Hardy & Grzegorz

Cyrogenic Control Valves Detail



Exhaust Gas Heating

example calculation external heat exchanger

HTRI		Final Results		Page 2	
		Released to the following HTRI Member Company: Gerd Lannewehr Gerd Lannewehr			
Xist Ver. 5.00 10.11.2006 08:22 SN: 1500212265				SI Units	
Wärmetauscher Argon/Wasser am Kryostat Gerda Max Planck Institut Kernphysik Rating - Horizontal Multipass Flow TEMA BEU Shell With Single-Segmental Baffles					
Process Data		Hot Shellside		Cold Tubeside	
Fluid name		Water		Argon	
Fluid condition		Sens. Liquid		Sens. Gas	
Total flow rate (kg/s)		22,8898		4,0000	
Weight fraction vapor, In/Out (—)		0,000	0,000	1,000	1,000
Temperature, In/Out (Deg C)		20,00	16,00	-180,00	5,00
Temperature, Average/Skin (Deg C)		18,0	16,72	-87,5	16,09
Wall temperature, Min/Max (Deg C)		13,24	18,66	12,23	18,10
Pressure, In/Average (kPa)		150,002	146,332	150,002	146,998
Pressure drop, Total/Allowed (kPa)		7,340		6,007	
Velocity, Mid/Max allow (m/s)		0,29		17,62	
Mole fraction inert (—)					
Average film coef. (W/m2-K)		3177,38		74,16	
Heat transfer safety factor (—)		1,000		1,000	
Fouling resistance (m2-K/W)		0,000000		0,000000	
Overall Performance Data					
Overall coef., Reqd/Clean/Actual (W/m2-K)		54,96	/	60,10	/ 60,10
Heat duty, Calculated/Specified (MegaWatts)		0,3839	/		
Effective overall temperature difference (Deg C)		67,4			
EMTD = (MTD) * (DELTA) * (F/G/H) (Deg C)		67,50	*	0,9985	* 1,0000
See Runtime Messages Report for warnings.					
Exchanger Fluid Volumes					
Approximate shellside (L)		894,6			
Approximate tubeside (L)		1819,6			
Shell Construction Information					
TEMA shell type		BEU	Shell ID	(mm)	800,000
Shells Series		1 Parallel	1	Total area	(m2) 105,290
Passes Shell		1 Tube	2	Eff. area	(m2/shell) 103,644
Shell orientation angle (deg)		0,00			
Impingement present		No			

Heater à la Icarus **not** possible:

- 6 containers of $h=5\text{m}$, $\varnothing=0.8\text{m}$, filled with silicate half-spheres, electrically heated
- in case no electric cooling of LAr,
- for $700\text{ Nm}^3/\text{h}$ LAr gas flow
- cost 150 kEuro

GERDA needs $8000\text{ Nm}^3/\text{h}$ heater
only known option: water reservoir

1) external heat exchanger

4 kg/s of LAr = $8600\text{ Nm}^3/\text{h}$

--> 22 kg/s water, $\varnothing=0.8\text{m}$, $h=5\text{m}$

105 m^2 heat exchanger surface

2) internal heat exchanger

- same construction

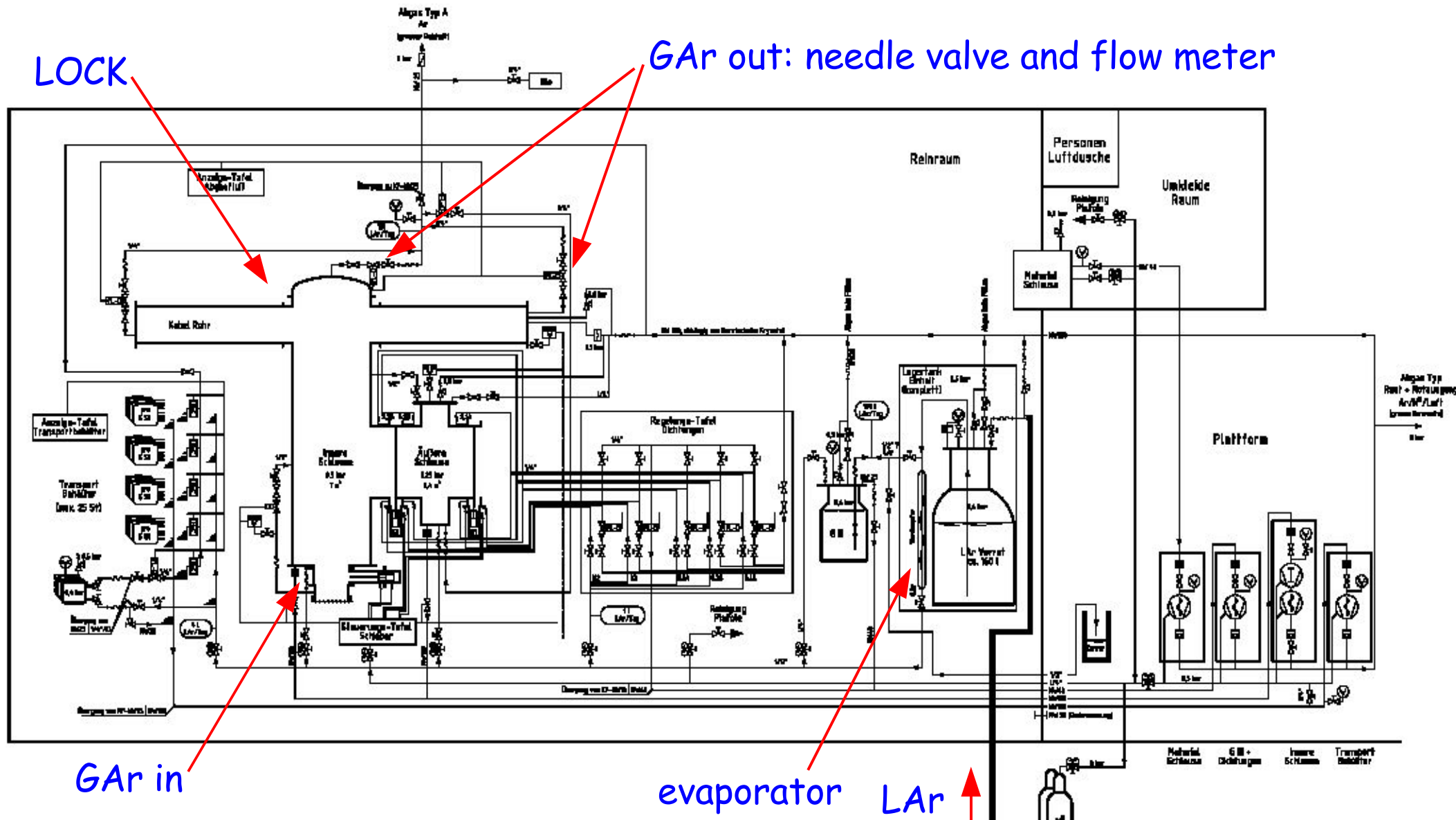
- 330 m of $\varnothing=0.1\text{m}$ pipe

3) pipes on outer surf. of water tank
 $\varnothing=10\text{m}$, $h=3.3\text{ m}$

Current Design of Penthouse Gas System

LOCK

GA₂ out: needle valve and flow meter



(variable) flow of GAr for Rn purging will modify gas pressure of cryostat
--> gas flow rate should be controlled by SPS of cryostat

Tendering

What is needed for start of tendering:

- feedback from NIER / LNGS concerning modifications of PID
- finalize PID:
 - include Rn purification
 - connection to penthouse gas system,
 - location of LAr & LN2 storage tanks
 - location of Rn purification, valves, ...
 - specify valves
 - pipe diameters, ...
- write tender document
- buy material delivered by MPI

Start tender early next year (German wide tendering)

Exhaust gas heater is a separate project:

- currently all (water) solutions 1-3 are dimensioned & conceptually designed
- should decide early next year (?)